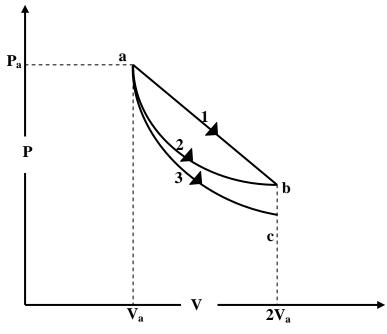
Outline Solutions to Coursework 3 : Week 3

QUESTION 1: (10 marks)



This is the same series of paths that were considered in week 2 exercises when the work and internal energy changes were calculated for each of the three paths.

<u>Path 1.</u>

From week 2 we found that

$$\Delta W_{1} = -\int_{V_{a}}^{2V_{a}} \left(-\frac{P_{a}}{2V_{a}}V + \frac{3}{2}P_{a} \right) dV = -0.75P_{a}V_{a}$$

and

$$\Delta U_1 = \frac{3}{2} (P_b V_b - P_a V_a) = \frac{3}{2} \left[\frac{P_a}{2} 2V_a - P_a V_a \right] = 0$$

We find from this the heat flow by using the first law as follows

<u>Path 2</u>

From week 2 we found that

$$\Delta W_2 = -P_a V_a \log_e 2 = -0.693 P_a V_a$$

and

$$\Delta U = \frac{3}{2} (P_b V_b - P_a V_a) = \frac{3}{2} \left[\frac{P_a}{2} 2 V_a - P_a V_a \right] = 0$$

We find from this the heat flow by using the first law as follows;

$$\Delta Q_2 = \Delta U_2 - \Delta W_2 = 0 + 0.693 P_a V_a = +0.693 P_a V_a$$
[3mks]

<u>Path 3</u>

From week 2 we found that

$$\Delta W_3 = -0.555 P_a V_a$$

and

$$\Delta U_3 = -0.555 P_a V_a$$

We find from this the heat flow by using the first law as follows;

$$\Delta Q_3 = \Delta U_3 - \Delta W_3 = -0.555 P_a V_a + 0.555 P_a V_a = 0$$
 [2mks]

as we would expect for an adiabatic process.

QUESTION 2: (14 Marks)

(a) From $PV^{\gamma} = c$ we can express the pressure as $P = cV^{-\gamma}$ Then the work calculation is

$$\mathcal{A}W_1 = -\int_{V_1}^{V_2} P dV = -c \int_{V_1}^{V_2} V^{-\gamma} dV = -c \left[\frac{-V^{-\gamma+1}}{\gamma-1} \right]_{V_1}^{V_2}$$
 [3mks]

and using $P = cV^{-\gamma}$ gives

$$\Delta W_{1} = \frac{1}{\gamma - 1} \left[P_{2} V_{2} - P_{1} V_{1} \right]$$
 [4mks]

(**b**) For monatomic argon $\gamma_{Ar} = \frac{5}{3}$ while for diatomic nitrogen $\gamma_{N_2} = \frac{7}{5}$. In an adiabatic process $P_a V_a^{\gamma} = P_b V_b^{\gamma}$ and if $V_b = 3V_a$, $P_b = (3^{-\gamma})P_a$. Remembering that in any process Work BY gas = -Work ON gas

we can use the result in (a) to calculate for argon

Work BY Argon =
$$-\left(\frac{1}{\frac{5}{3}-1}\right)(P_bV_b - P_aV_a) = \frac{3}{2}\left[1-3^{-\frac{2}{3}}\right]P_aV_a = 0.779P_aV_a$$
[3mks]

and for nitrogen we obtain

Work BY Nitrogen =
$$-\left(\frac{1}{\frac{7}{5}-1}\right)(P_bV_b - P_aV_a) = \frac{5}{2}\left[1-3^{-\frac{2}{5}}\right]P_aV_a = 0.889P_aV_a$$
[3mks]

Thus the diatomic gas does more work on the surroundings. [1mk]

QUESTION 3:(16 marks)

(a)

$$PV^{\gamma} = PVV^{\gamma-1} = nRTV^{\gamma-1} = const \implies$$

thus the adiabatic law can also be written as

$$TV^{\gamma-1} = const$$
 [2mks]

For
$$\gamma = \frac{7}{5}$$
, $TV^{2/5} = const$ or $T = \frac{c}{V^{2/5}}$.

For a small volume change, $\Delta T \approx \left(\frac{dT}{dV}\right)_{adiabatic} \times \Delta V$

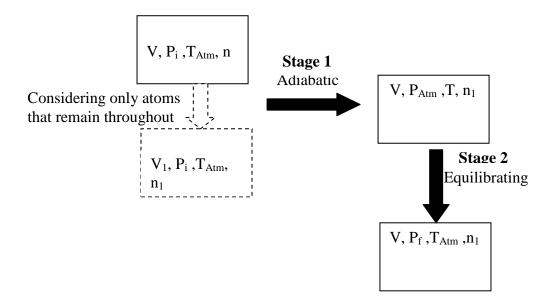
$$\left(\frac{dT}{dV}\right)_{adiabatic} = -\frac{2}{5}\frac{c}{\frac{7}{5}} = -\frac{2}{5}\frac{T}{V}$$
 [2mks]

thus

$$\Delta T \approx \left(\frac{dT}{dV}\right)_{adiabatic} \times \Delta V \approx -\frac{2}{5} (300 \ K) ((-0.1) = +12 \ K$$
 [4mks]

(b)

(i) There are three systems to use throughout the two stage process;



1) the initial state, tyre is at T_{atm} and P_i

2) the state immediately after the valve is opened and shut, T, P_{atm}

and

3) the final equilibrium state, T_{atm} , P_f

Let *V* be the fixed total volume of the tyre and let V_1 be the initial volume of gas which remains inside the tire throughout. We can apply the equation of state to each stage for the n_1 moles of gas which remain inside .

NB. We are using the fact that V and n are extensive variables and in general we can divide any volume V of a gas with n molecules into (V_1, n_1) and (V_2, n_2) and write $PV_1 = n_1RT$ and $PV_2 = n_2RT$ (P and T are intensive variables being the same in each of the divided volumes).

Thus in **stage 1**, $P_iV_l = n_lRT_{Atm}$ (and $P_iV = nRT_{Atm}$)

in stage 2, $P_{Atm}V = n_1RT$, where *T* is some intermediate temperature immediately following the expansion of the gas.

and in **stage 3** finally $P_f V = n_I R T_{Atm}$.

Stage 1 to stage 2 is an adiabatic process, $PV^{\gamma} = const$ or equivalently $P^{1/\gamma}V = const$ by taking root γ on both sides of the equation, but only if we compare systems with the same number of moles *n* (or molecules) ie for our initial system only the sub-volume V_1 containing n_1 moles so we can write $P_i^{1/\gamma}V_1 = P_{atm}^{1/\gamma}V$ and use the equation of state to change the variables

$$P^{1/\gamma}V = P^{1/\gamma-1}PV = P^{1/\gamma-1}n_1RT = const$$

Thus the adiabatic law in terms of pressure and temperature is

$$P^{\frac{1}{\gamma}-1}T = const$$
 [1mk]

Remember the constant is generally not the same constant!

As we go from stage 1 to stage 2 adiabatically we can write

$$P_{i}^{1/\gamma-1}T_{Atm} = P_{Atm}^{1/\gamma-1}T$$
 [1mk]

whence

$$\frac{T}{T_{Atm}} = \left(\frac{P_i}{P_{Atm}}\right)^{1/\gamma - 1} = \left(\frac{P_i}{P_{Atm}}\right)^{-2/\gamma}$$

If $P_i = 4$ atm, then $T = T_{Atm} \times 4^{-2/7} = 0.673 T_{Atm}$ [2mks]

ii) Now we compare stage 1 with stage 3,

NB. In comparing stages 1 and 3 we need to take care in using equations of state and adiabatic rule as there is a different number of molecules present in stage 1 and 3 (some were lost when the valve was opened). To apply the equations equally to stages 1 and 2 (or 3) we need only consider in stage 1 the volume V_1 containing the molecules n_1

From the equation of state we will have

$$P_i V_1 = P_f V$$

Or equivalently

$$\frac{P_i}{P_f} = \frac{V}{V_1}$$

However, from stage 1 to stage 2 we have the adiabatic relation $P_i V_1^{\gamma} = P_{Atm} V^{\gamma}$ Thus

$$\frac{P_i}{P_{Atm}} = \left(\frac{V}{V_1}\right)^{\gamma} = \left(\frac{P_i}{P_f}\right)^{\gamma}$$
[1mk]

Taking logs

$$ln\left(\frac{P_{i}}{P_{Atm}}\right) = \gamma ln\left(\frac{P_{i}}{P_{f}}\right)$$

$$\gamma = \frac{ln\left(\frac{P_{i}}{P_{Atm}}\right)}{ln\left(\frac{P_{i}}{P_{f}}\right)}$$
[3mks]